

VERSION: 2.4

4/15/2010

Manufacturer: Arada

Model: Farrington 16

Date: 2/21/2017

Run: 5

Control #: 035-S-075-1

Test Duration: 120

Burn Category: 4

Wood Moisture (% DRY):

19.9

Wood Moisture (% wet):

16.60

Load Weight (lb wet):

10.60

Burn Rate (dry kg/h):

2.01

Total Particulate Emissions:

3.36

g

Appliance Type:

Cat

(Cat, Non-Cat, Pe

Temp. Units

F

(F or C)

Weight Units

lb

(kg or lb)

Fuel Data

D. Fir

HHV

19,810

kJ/kg

%C

48.73

%H

6.87

%O

43.90

%Ash

0.50

Averages

482.3

71.5

11.14

9.51

0.29

Temp. (F)

Elapsed
Time (min)

Fuel Weight
Remaining (lb)

Flue
Gas

Room
Temp

Flue Gas Composition (%)
O2 CO2 CO

0	10.6	451.0	70.0	15.33	5.05	0.13
10	8.4	588.0	70.0	2.16	18.46	1.65
20	5.9	610.0	70.0	1.85	19.24	0.90
30	4.4	553.0	70.0	9.32	12.11	0.04
40	3.1	543.0	71.0	9.89	11.33	0.04
50	2.3	505.0	70.0	12.31	8.47	0.08
60	1.8	473.0	71.0	13.06	7.52	0.11
70	1.3	454.0	72.0	13.09	7.50	0.11
80	1.0	441.0	73.0	13.73	6.49	0.17
90	0.6	428.0	73.0	13.13	7.23	0.15
100	0.4	415.0	73.0	13.47	6.91	0.15
110	0.2	407.0	73.0	13.56	6.85	0.14
120	0.0	402.0	73.0	13.88	6.51	0.14

ellet)

☒ Dougla

☐ Oak

Manufacturer: Arada
 Model: Farringdon 16
 Date: 2/21/2017
 Run: 5
 Control #: 035-S-075-1
 Test Duration: 120 min

	HHV	LHV
Eff	71.7%	77.5%
Comb Eff	96.8%	96.8%
HT Eff	74.1%	80.1%
Output	28,489	kJ/h
Burn Rate	2.01	kg/h
Grams CO	183	g
Input	39,731	kJ/h
MC wet	16.60	
Averages	0.29	9.51

Ultimate CO:
 CO2-ult 19.64
 Fo
 1.062

INPUT DATA				Oxygen Calculation			Input
Elapsed Time	Weight Remaining (kg)	% CO [e]	% CO2 [d]	Excess Air EA	Total O2	Calc. % O2 [g]	Flue Gas (°C)
0	4.81	0.13	5.05	279.2%	20.60	15.48	232.8
10	3.81	1.65	18.46	-2.3%	19.61	0.33	308.9
20	2.68	0.90	19.24	-2.5%	19.61	-0.08	321.1
30	2.00	0.04	12.11	61.7%	20.14	8.01	289.4
40	1.41	0.04	11.33	72.8%	20.19	8.84	283.9
50	1.04	0.08	8.47	129.7%	20.38	11.87	262.8
60	0.82	0.11	7.52	157.4%	20.44	12.86	245.0
70	0.59	0.11	7.50	158.1%	20.44	12.88	234.4
80	0.45	0.17	6.49	194.9%	20.50	13.93	227.2
90	0.27	0.15	7.23	166.2%	20.45	13.15	220.0
100	0.18	0.15	6.91	178.2%	20.47	13.49	212.8
110	0.09	0.14	6.85	181.0%	20.48	13.56	208.3
120	0.00	0.14	6.51	195.4%	20.50	13.92	205.6
0							

Overall Heating Efficiency:	71.7%	Air Fuel Ratio (A/F)		
Combustion Efficiency:	96.8%	Dry Molecular Weight (Md)	29.95	%HC 0.88
Heat Transfer Efficiency:	74.1%	Dry Moles Exhaust Gas (Nr):	397.71	
		Air Fuel Ratio (A/F)	11.40	

Heat Output: 27,025 Btu/h 28,489 kJ/h

Burn Duration: 2 h

Stack Temp: 484.9 Deg. F 251.6 Deg. C

Combustion Efficiency: 96.8%
 Total Input (kJ): 79,462 75,366 (Btu)
 Total Output (kJ): 56,978 54,041 (Btu)
 Efficiency: 71.7%
 Total CO (g): 183.05

Load Weight (kg):
 Fuel Heating:
 Value in kJ/kg - CV:

80212	4.06	6.87	2.74	19810.00	16.60	79.56	21.10	2.42
Fuel Properties			Oxygen /16= [c]	Calorific Value	Mw Moisture Fuel Burnt	Mass Balance (moles/100 mole dry		
Total Input	Carbon /12= [a]	Hydrogen /1= [b]				[h]	[u]	[w]
0	4.06	6.87	2.74	19810.00	16.60	79.34	21.04	1.27
25863	4.06	6.87	2.74	19810.00	16.60	79.56	21.10	5.01
14993	4.06	6.87	2.74	19810.00	16.60	79.94	21.20	4.99
10495	4.06	6.87	2.74	19810.00	16.60	79.84	21.18	2.99
7871	4.06	6.87	2.74	19810.00	16.60	79.79	21.16	2.80
4873	4.06	6.87	2.74	19810.00	16.60	79.58	21.11	2.10
3748	4.06	6.87	2.74	19810.00	16.60	79.51	21.09	1.88
2999	4.06	6.87	2.74	19810.00	16.60	79.51	21.09	1.87
2624	4.06	6.87	2.74	19810.00	16.60	79.41	21.06	1.64
2249	4.06	6.87	2.74	19810.00	16.60	79.47	21.08	1.82
1499	4.06	6.87	2.74	19810.00	16.60	79.45	21.07	1.74
2249	4.06	6.87	2.74	19810.00	16.60	79.45	21.07	1.72
750	4.06	6.87	2.74	19810.00	16.60	79.43	21.07	1.64

Moisture Content MCwb: 16.60

Moisture of Wood (wet basis): 16.60
Initial Dry Weight Wtdo (kg): 4.01
Moisture Content Dry 19.90

Dry kg : 4.01
CA: 48.73
HY: 6.87
OX: 43.90

4.81
HHV LHV HHV LHV
19810.00 18328.69 Btu/lb 8522.48 7885.21

8.27	0.03	0.24	39.82	59.74	0.95	0.04	390.04	34.44
: flue gas)		kg Wood per 100 mole dfp	Moles per kg of Dry Wood					
[j]	[k]	Nk	CO2	O2	CO	HC	N2	H2O
4.39	-0.01	0.13	39.83	122.13	1.03	-0.05	625.80	34.62
16.73	0.24	0.50	37.02	0.66	3.31	0.48	159.57	33.56
16.88	0.13	0.50	38.74	-0.16	1.81	0.26	160.94	33.99
10.29	-0.01	0.30	40.70	26.91	0.13	-0.02	268.35	34.57
9.63	-0.01	0.28	40.70	31.75	0.14	-0.03	286.62	34.58
7.24	-0.01	0.21	40.47	56.69	0.38	-0.04	380.22	34.59
6.46	0.00	0.19	40.25	68.84	0.59	-0.02	425.55	34.57
6.44	0.00	0.19	40.25	69.13	0.59	-0.03	426.66	34.57
5.63	0.00	0.16	39.76	85.30	1.04	0.01	486.48	34.49
6.24	0.00	0.18	39.98	72.70	0.83	0.00	439.45	34.51
5.97	0.00	0.17	39.94	77.97	0.87	0.00	459.28	34.52
5.91	0.00	0.17	40.00	79.18	0.82	-0.01	463.99	34.54
5.63	0.00	0.16	39.97	85.46	0.86	-0.01	487.62	34.55

11.06	523.32	9471.59	6959.91	6726.68	6660.80	9486.04	8036.41	295.07
Moisture Present	Stack Temp K	Heat Content Change - Ambient to Stack Temperature Flue Gas Constituent						Room Temp K
		CO2	O2	CO	N2	CH4	H2O	
11.06	505.93	8708.55	6431.04	6223.54	6160.89	8652.15	7437.87	294.26
11.06	582.04	12157.56	8842.07	8522.72	8444.13	12376.57	10174.80	294.26
11.06	594.26	12727.07	9234.11	8894.96	8814.13	13004.89	10617.39	294.26
11.06	562.59	11260.45	8221.16	7932.25	7857.40	11394.23	9472.45	294.26
11.06	557.04	10984.99	8028.03	7747.93	7674.39	11098.02	9252.98	294.82
11.06	535.93	10047.95	7375.15	7125.91	7056.57	10081.44	8512.72	294.26
11.06	518.15	9229.92	6798.34	6574.56	6509.32	9208.94	7855.96	294.82
11.06	507.59	8739.95	6450.57	6241.52	6178.89	8691.36	7459.07	295.37
11.06	500.37	8399.88	6208.03	6008.96	5948.22	8334.67	7181.82	295.93
11.06	493.15	8082.49	5982.31	5792.70	5733.67	8000.35	6924.05	295.93
11.06	485.93	7766.61	5757.07	5576.73	5519.45	7668.96	6666.58	295.93
11.06	481.48	7572.98	5618.69	5443.97	5387.79	7466.48	6508.29	295.93
11.06	478.71	7452.25	5532.29	5361.05	5305.56	7340.49	6409.41	295.93

SUMS							AVERAGE
4893.32	4928.96	3597.41	32054.24	504.53	23278.28	7474.39	5902.39
Energy Losses (kJ/kg of Dry Fuel)							Total
Flue Gas Constituent							Loss
CO2	O2	CO	N2	CH4	H2O Comb	H2O Fuel MC	Rate
346.90	785.41	296.51	3855.51	-42.26	1779.53	568.34	7589.94
450.10	5.80	964.66	1347.39	434.40	1817.07	598.59	5618.00
493.00	-1.48	528.89	1418.58	238.78	1855.60	603.49	5136.86
458.32	221.26	39.11	2108.53	-21.37	1847.47	590.83	5244.16
447.08	254.90	41.78	2199.63	-27.16	1840.57	588.40	5345.19
406.60	418.08	110.88	2683.03	-31.95	1815.53	580.22	5982.39
371.49	467.97	170.48	2770.02	-22.42	1791.72	572.96	6122.22
351.76	445.94	170.73	2636.29	-22.63	1778.02	568.57	5928.69
333.95	529.57	300.96	2893.68	13.08	1764.37	565.51	6401.12
323.13	434.92	239.53	2519.66	3.54	1756.56	562.66	5840.00
310.23	448.90	250.22	2534.97	0.85	1747.98	559.81	5852.96
302.94	444.88	235.82	2499.86	-7.37	1743.44	558.06	5777.63
297.83	472.80	247.83	2587.09	-10.96	1740.42	556.97	5891.97

SUMS						
22484	2551	19932.91	57727	2551	183.05	12.60
Total Loss	Chemical Loss 1	Sensible and Latent Loss	Total Output	Chem Loss 2	Grams Produced	
					CO	HC
0	0	0.00	0	0	0.00	0.00
7334	1782	5552.58	18528	1782	120.96	10.05
3888	566	3321.53	11105	566	38.40	3.20
2778	9	2769.28	7717	9	1.99	-0.20
2124	5	2118.34	5747	5	1.60	-0.19
1471	19	1452.66	3401	19	2.63	-0.14
1158	27	1131.05	2590	27	3.12	-0.08
897	22	875.51	2101	22	2.50	-0.06
848	41	807.05	1776	41	3.86	0.03
663	27	635.94	1586	27	2.64	0.01
443	19	424.34	1056	19	1.84	0.00
656	25	630.47	1593	25	2.60	-0.01
223	9	214.17	527	9	0.91	-0.01

Dirigo Laboratories, Inc.

Manufacturer: Arada
Model: Farringdon 16
Date: 2/21/2017
Run: 5
Control #: 035-S-075-1
Test Duration: 120
Output Category: 4

	HHV Basis	LHV Basis
Overall Efficiency	71.7%	77.5%
Combustion Efficiency	96.8%	96.8%
Heat Transfer Efficiency	74.1%	80.1%

HHV Output Rate (kJ/h)	28,489	27,025	(Btu/h)
Burn Rate (kg/h)	2.01	4.42	(lb/h)
Input (kJ/h)	39,731	37,689	(Btu/h)

Test Load Weight (dry kg)	4.0	8.8	dry lb
MC wet (%)	16.60		
MC dry (%)	19.90		
Particulate (g)	3.36		
CO (g)	183		
Test Duration (h)	2		

Emissions	Particulate	CO
g/MJ Output	0.06	3.21
g/kg Dry Fuel	0.84	45.64
g/h	1.68	91.53
lb/MM Btu Output	0.14	7.47

Air/Fuel Ratio (A/F)	11.40
----------------------	-------

Test Results in Accordance with CSA B415.1-10

Default Fuel Values

	D. Fir	Oak
HHV (kJ/kg)	19,810	19,887
%C	48.73	50
%H	6.87	6.6
%O	43.9	42.9
%Ash	0.5	0.5